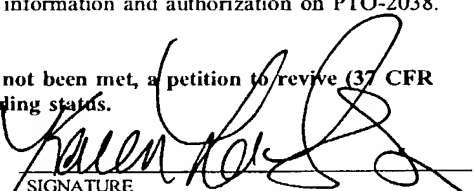


JC07 Rec'd PCT/PTO 19 FEB 2002

FORM PTO-1390 (REV. 12-2001)		U.S. DEPARTMENT OF COMMERCE PATENT AND TRADEMARK OFFICE	ATTORNEY'S DOCKET NUMBER 09100.024
TRANSMITTAL LETTER TO THE UNITED STATES DESIGNATED/ELECTED OFFICE (DO/EO/US) CONCERNING A FILING UNDER 35 U.S.C. 371			U.S. APPLICATION NO. (If known, see 37 CFR 1.5) 10/049879
INTERNATIONAL APPLICATION NO. PCT/GB00/03149	INTERNATIONAL FILING DATE 15 AUGUST 2000	PRIORITY DATE CLAIMED 19 AUGUST 1999	
TITLE OF INVENTION CONTAINER PRODUCTION PROCESS			
APPLICANT(S) FOR DO/EO/US Jorunn NILSEN et al.			
Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:			
<p>1. <input checked="" type="checkbox"/> This is a FIRST submission of items concerning a filing under 35 U.S.C. 371.</p> <p>2. <input type="checkbox"/> This is a SECOND or SUBSEQUENT submission of items concerning a filing under 35 U.S.C. 371.</p> <p>3. <input type="checkbox"/> This is an express request to begin national examination procedures (35 U.S.C. 371(f)). The submission must include items (5), (6), (9) and (21) indicated below.</p> <p>4. <input checked="" type="checkbox"/> The US has been elected by the expiration of 19 months from the priority date (Article 31).</p> <p>5. <input checked="" type="checkbox"/> A copy of the International Application as filed (35 U.S.C. 371(c)(2))</p> <p style="margin-left: 20px;">a. <input checked="" type="checkbox"/> is attached hereto (required only if not communicated by the International Bureau).</p> <p style="margin-left: 20px;">b. <input checked="" type="checkbox"/> has been communicated by the International Bureau.</p> <p style="margin-left: 20px;">c. <input type="checkbox"/> is not required, as the application was filed in the United States Receiving Office (RO/US).</p> <p>6. <input type="checkbox"/> An English language translation of the International Application as filed (35 U.S.C. 371(c)(2)).</p> <p style="margin-left: 20px;">a. <input type="checkbox"/> is attached hereto.</p> <p style="margin-left: 20px;">b. <input type="checkbox"/> has been previously submitted under 35 U.S.C. 154(d)(4)</p> <p>7. <input checked="" type="checkbox"/> Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371(c)(3))</p> <p style="margin-left: 20px;">a. <input checked="" type="checkbox"/> are attached hereto (required only if not communicated by the International Bureau).</p> <p style="margin-left: 20px;">b. <input checked="" type="checkbox"/> have been communicated by the International Bureau.</p> <p style="margin-left: 20px;">c. <input type="checkbox"/> have not been made; however, the time limit for making such amendments has NOT expired.</p> <p style="margin-left: 20px;">d. <input type="checkbox"/> have not been made and will not be made.</p> <p>8. <input type="checkbox"/> An English language translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371 (c)(3)).</p> <p>9. <input type="checkbox"/> An oath or declaration of the inventor(s) (35 U.S.C. 371(c)(4)).</p> <p>10. <input type="checkbox"/> An English language translation of the annexes of the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371(c)(5)).</p> <p>Items 11 to 20 below concern document(s) or information included:</p> <p>11. <input type="checkbox"/> An Information Disclosure Statement under 37 CFR 1.97 and 1.98.</p> <p>12. <input type="checkbox"/> An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included.</p> <p>13. <input checked="" type="checkbox"/> A FIRST preliminary amendment.</p> <p>14. <input type="checkbox"/> A SECOND or SUBSEQUENT preliminary amendment.</p> <p>15. <input type="checkbox"/> A substitute specification.</p> <p>16. <input type="checkbox"/> A change of power of attorney and/or address letter.</p> <p>17. <input type="checkbox"/> A computer-readable form of the sequence listing in accordance with PCT Rule 13ter.2 and 35 U.S.C. 1.821 - 1.825.</p> <p>18. <input type="checkbox"/> A second copy of the published international application under 35 U.S.C. 154(d)(4).</p> <p>19. <input type="checkbox"/> A second copy of the English language translation of the international application under 35 U.S.C. 154(d)(4).</p> <p>20. <input type="checkbox"/> Other items or information:</p>			

U.S. APPLICATION NO. 10/049879 INTERNATIONAL APPLICATION NO. PCT/GB00/03149		ATTORNEY'S DOCKET NUMBER 09100.024	
21. <input type="checkbox"/> The following fees are submitted: BASIC NATIONAL FEE (37 CFR 1.492 (a) (1) - (5)): Neither international preliminary examination fee (37 CFR 1.482) nor international search fee (37 CFR 1.445(a)(2)) paid to USPTO and International Search Report not prepared by the EPO or JPO. \$1040.00 International preliminary examination fee (37 CFR 1.482) not paid to USPTO but International Search Report prepared by the EPO or JPO \$890.00 International preliminary examination fee (37 CFR 1.482) not paid to USPTO but international search fee (37 CFR 1.445(a)(2)) paid to USPTO \$740.00 International preliminary examination fee (37 CFR 1.482) paid to USPTO but all claims did not satisfy provisions of PCT Article 33(1)-(4) \$710.00 International preliminary examination fee (37 CFR 1.482) paid to USPTO and all claims satisfied provisions of PCT Article 33(1)-(4) \$100.00 ENTER APPROPRIATE BASIC FEE AMOUNT =		CALCULATIONS PTO USE ONLY	
Surcharge of \$130.00 for furnishing the oath or declaration later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492(e)).		\$ 890⁰⁰ \$ 130⁰⁰	
CLAIMS	NUMBER FILED	NUMBER EXTRA	RATE
Total claims	- 20 =		x \$18.00
Independent claims	- 3 =		x \$84.00
MULTIPLE DEPENDENT CLAIM(S) (if applicable)		+	\$280.00
TOTAL OF ABOVE CALCULATIONS =		\$ 1020⁰⁰	
<input type="checkbox"/> Applicant claims small entity status. See 37 CFR 1.27. The fees indicated above are reduced by 1/2.		\$ — +	
SUBTOTAL =		\$ 1020⁰⁰	
Processing fee of \$130.00 for furnishing the English translation later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492(f)).		\$ —	
TOTAL NATIONAL FEE =		\$ 1020⁰⁰	
Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31). \$40.00 per property +		\$ —	
TOTAL FEES ENCLOSED =		\$ 1020⁰⁰	
Amount to be refunded:		\$	
charged:		\$	
a. <input checked="" type="checkbox"/> A check in the amount of \$ 1020⁰⁰ to cover the above fees is enclosed. b. <input type="checkbox"/> Please charge my Deposit Account No. _____ in the amount of \$ _____ to cover the above fees. A duplicate copy of this sheet is enclosed. c. <input checked="" type="checkbox"/> The Commissioner is hereby authorized to charge any additional fees which may be required, or credit any overpayment to Deposit Account No. 50-0548 . A duplicate copy of this sheet is enclosed. d. <input type="checkbox"/> Fees are to be charged to a credit card. WARNING: Information on this form may become public. Credit card information should not be included on this form. Provide credit card information and authorization on PTO-2038.			
NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR 1.137 (a) or (b)) must be filed and granted to restore the application to pending status.			
SEND ALL CORRESPONDENCE TO Karen Lee Orzechowski Liniak, Berenato, Longacre & White, 6550 Rock Spring Drive Suite 240 Bethesda, MD 20817		 SIGNATURE Karen Lee Orzechowski NAME 31,621 REGISTRATION NUMBER	

Attorney's Docket No. 09100.024

PATENT**IN THE UNITED STATES PATENT AND TRADEMARK OFFICE**

In re: Jorunn NILSEN et al.
Appl. No.: [National Stage of PCT/GB00/03149] Group Art Unit: [Not Assigned]
Filed: February 19, 2002 Examiner: [Not Assigned]
For: CONTAINER PRODUCTION PROCESS

PRELIMINARY AMENDMENT

Assistant Commissioner for Patents
Washington, DC 20231

Sir:

Prior to calculating the filing fee for the above-identified patent application, please amend the application as follows:

In the Claims:

Please amend claims 3 and 4 to read as follows:

3. (Amended) A process as claimed in claim 1, wherein said HDPE has a density of 945 to 975 kg/m³.

4. (Amended) A process as claimed in claim 1 wherein said HDPE has a density of to 960 kg/m³, a weight average molecular weight of 250000 to 350000 D, a number average molecular weight of 7000 to 18000 D, a molecular weight distribution of 18 to 50, an MFR₂₁ of 3 to 8 g/10 min, a tensile modulus of at least 900 mPa, and a comonomer content of 1 to 2 wt. %.

Please add new claims 8-10 as follows:

8. A process as claimed in claim 2, wherein said HDPE has a density of 945 to 975 kg/m³.

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9. A process as claimed in claim 2 wherein said HDPE has a density of to 960 kg/m³, a weight average molecular weight of 250000 to 350000 D, a number average molecular weight of 7000 to 18000 D, a molecular weight distribution of 18 to 50, an MFR₂₁ of 3 to 8 g/10 min, a tensile modulus of at least 900 mPa, and a comonomer content of 1 to 2 wt. %.

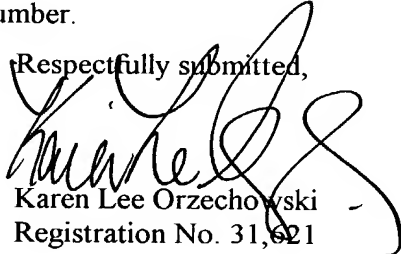
10. A process as claimed in claim 3 wherein said HDPE has a density of to 960 kg/m³, a weight average molecular weight of 250000 to 350000 D, a number average molecular weight of 7000 to 18000 D, a molecular weight distribution of 18 to 50, an MFR₂₁ of 3 to 8 g/10 min, a tensile modulus of at least 900 mPa, and a comonomer content of 1 to 2 wt. %.

REMARKS

These amendments are made solely for the purposes of eliminating multiple dependencies. No new matter has been added.

Should the Examiner has any questions or wishes to discuss this application, kindly telephone the undersigned at the below-listed number.

Respectfully submitted,


 Karen Lee Orzechowski
 Registration No. 31,621

Date: February 19, 2002

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CERTIFICATION OF FACSIMILE TRANSMISSION	CERTIFICATE OF MAILING
<p>I hereby certify that this paper is being facsimile transmitted to the Patent and Trademark Office at Fax No. (703) 308-2742 on February 19, 2002.</p> <p>_____ Karen Lee Orzechowski</p>	<p>I hereby certify that this correspondence is being deposited with the United States Postal Service with sufficient postage as first class mail in an envelope addressed to: Assistant Commissioner For Patents, Washington, DC 20231, on February 19, 2002.</p> <p>_____ Karen Lee Orzechowski</p>

Preliminary Amendment
 Application No. [National Stage of PCT/GB00/03149]
 Filing Date: February 19, 2002
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APPENDIX

3. (Amended) A process as claimed in [either of claims 1 and 2] claim 1, wherein said HDPE has a density of 945 to 975 kg/m³.

4. (Amended) A process as claimed in [any one of claims 1 to 3] claim 1 wherein said HDPE has a density of to 960 kg/m³, a weight average molecular weight of 250000 to 350000 D, a number average molecular weight of 7000 to 18000 D, a molecular weight distribution of 18 to 50, an MFR₂₁ of 3 to 8 g/10 min, a tensile modulus of at least 900 mPa, and a comonomer content of 1 to 2 wt. %.

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9919718.8 **19 August 1999 (19.08.1999)** **GB**
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- (81) Designated States (*national*): **AE, AG, AL, AM, AT, AT (utility model), AU, AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CR, CU, CZ, CZ (utility model), DE, DE (utility model), DK, DK (utility model), DM, DZ, EE, EE (utility model), ES, FI, FI (utility model), GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KR (utility model), KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SK (utility model), SL, TJ, TM, TR, TT, TZ, UA, UG, US, UZ, VN, YU, ZA, ZW.**
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- Published:**
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(54) Title: **CONTAINER PRODUCTION PROCESS**

(57) Abstract: The invention provides the use of bimodal HDPE in the production by blow moulding of medium to large volume containers having improved environmental stress crack resistance.

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Container Production Process

This invention relates to improvements in and relating to the production of containers by blow moulding of a polymer material, in particular a high density polyethylene (HDPE).

In the production of containers using polymer materials, a variety of moulding techniques may be used, in particular blow moulding, slush moulding, injection moulding and rotational moulding. For very large containers, e.g. for use as oil or water tanks, rotational moulding is a preferred technique; however for medium to large sized containers, e.g. 8 to 250L volume, blow moulding is commonly used.

Generally in the blow moulding of containers a heated parison or extrudate is expanded to contact the interior surface of a mould by the action of pressurized gas within the parison and/or by application of a partial vacuum within the mould, e.g. by use of a mould having within its surface gas outlet vents through which a partial vacuum may be applied.

For blow moulding to be successful, the heated polymer must be able to stretch smoothly to produce a satisfactorily uniform skin in contact with the mould surface.

In the production of containers by blow moulding of polyethylene, the polymer used has typically been a high molecular weight (HMW) high density polyethylene (HDPE), generally with a melt flow rate (MFR₂₁) in the range 2 to 12 g/10 min. Such materials may be produced for example by chromium-catalysed ethylene polymerization. However the choice of such materials essentially represents a compromise between the properties of the polymer, in particular the processability properties required for the blow moulding to be performed efficiently and successfully and the mechanical and chemical properties

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required for the end uses of the blow moulded containers, e.g. impact resistance, stiffness, and environmental stress crack resistance (ESCR).

We have now found that large volume blow moulded containers which have excellent ESCR properties may be produced if one uses a high density polyethylene (HDPE) comprising at least two polyethylene components having different molecular weight distributions wherein at least one of said components is an ethylene copolymer. Such HDPE is referred to hereinafter as bimodal.

Thus viewed from one aspect the invention provides a process for the preparation of an at least 2L (e.g. 2 to 1000L, preferably 2 to 250L, more preferably 8 to 230L, still more preferably 30 to 225L) volume polyethylene container which process comprises blow moulding a bimodal HDPE.

In the process of the invention, the parison is conveniently part-blown before the mould is closed, the mould is then closed and the blowing of the parison is completed.

By polyethylene is meant a polymer the majority by weight of which derives from ethylene monomer units. While the different polyethylene components of the bimodal HDPE may all be ethylene copolymers, and while an ethylene homopolymer may be one of the components, the polyethylene components cannot all be ethylene homopolymers. Where one component is an ethylene homopolymer, this is preferably the component with the lower weight average molecular weight (M_w) and its M_w is preferably 5000 to 100000 D, more preferably 20000 to 40000 D. In the ethylene copolymer components, comonomer contributions, e.g. up to 20% by weight more preferably up to 10% by weight, may derive from other copolymerizable monomers, generally C_{3-20} , especially C_{3-10} , comonomers, particularly singly or multiply ethylenically unsaturated comonomers, in particular C_{3-10} α -olefins such as propene, but-1-ene, hex-1-ene, etc.

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(The term ethylene copolymer is used herein to relate to a polyethylene deriving from ethylene and one or more such copolymerizable comonomers). Moreover, the polyethylene may contain minor, e.g up to 10% by weight, preferably up to 5% by weight of other polymers, e.g. other polyolefins in particular polypropylenes, as well as additives such as plasticizers, colours, fillers, radiation stabilizers, antioxidants, etc., generally in amounts up to 10% by weight, preferably up to 5% by weight.

By HDPE is meant a polyethylene having a density of 940 to 980 kg/m³, preferably 945 to 975 kg/m³, more preferably 945 to 960 kg/m³, and a crystallinity of 60 to 95%, preferably 70 to 90%.

The HDPE used according to the invention is a bimodal or multimodal polymer. By bimodal (or multimodal), it is generally meant that the polymer consists of at least two fractions (components), one of which has a relatively low molecular weight and a relatively high density and another of which has a relatively high molecular weight and a relatively low density. Typically the molecular weight distribution (MWD) of a polymer produced in a single polymerization stage using a single monomer mixture, a single polymerization catalyst and a single set of process conditions (ie. temperature, pressure etc.) will show a single maximum, the breadth of which will depend on catalyst choice, reactor choice, process conditions, etc, ie. such a polymer will be monomodal.

A bimodal or multimodal polyethylene may be produced by blending two or more monomodal polyethylenes having differently centred maxima in their MWDs. Alternatively and preferably the bimodal polyethylene may be produced by polymerization using conditions which create a bimodal or multimodal polymer product, e.g. using a catalyst system or mixture with two or more different catalytic sites, using two or more stage

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polymerisation process with different process conditions in the different stages (e.g. different temperatures, pressures, polymerisation media, hydrogen partial pressures, etc). (See EP-A-778289)

Such a bimodal (or multimodal) HDPE may be produced relatively simply by a multistage ethylene polymerization, e.g. using a series of reactors, with comonomer addition in only the reactor(s) used for production of the higher/highest molecular weight component(s). Examples of bimodal PE production are given in EP-A-778289 and WO92/12182.

If an ethylene homopolymer component is produced by slurry polymerization involving use of recycled diluent, that diluent may contain small amounts of higher α -olefins as contaminants. Likewise where an earlier polymerization stage has produced an ethylene copolymer component, small amounts of comonomer may be carried over to an ethylene homopolymerization stage. Accordingly, by ethylene homopolymer is meant herein a polymer containing at least 99.9% by weight of ethylene units. Likewise as in a multistage/multireactor polymerization using more than one catalyst system, the homopolymerization catalysts may be at least partially active during the copolymerization reaction, any copolymer component making up less than 5% by weight of the total polymer shall not be considered to be the lowest molecular weight component in an HDPE according to the invention.

The copolymer component(s) of the HDPE used according to the invention will generally contain at least 0.1% by weight, preferably at least 0.5% by weight of non-ethylene monomer units, e.g. 0.5 to 6% of such comonomer units.

The polymerization reactions used to produce the HDPE of the invention may involve conventional ethylene homopolymerization or copolymerization reactions, e.g. gas-phase, slurry phase, liquid phase polymerizations,

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using conventional reactors, e.g. loop reactors, gas phase reactors, batch reactors etc. (see for example WO97/44371 and WO96/18662). The catalyst systems used may likewise be any conventional systems, e.g. chromium catalysts, Ziegler-Natta and metallocene or metallocene:aluminoxane catalysts, either homogeneous or more preferably heterogeneous catalysts, e.g. catalysts supported on inorganic or organic particulates, in particular on magnesium halides or inorganic oxides such as silica, alumina or silica-alumina. For the preparation of the high molecular weight component in particular it is especially desirable to use supported Ziegler-Natta catalysts as the molecular weight can then conveniently be controlled using hydrogen. It is also possible to use supported metallocene catalysts as it is particularly straightforward to select desired molecular weights by appropriate selection of particular metallocenes. The metallocenes used will typically be group IVa to VIa metals (in particular Zr or Hf) complexed by optionally substituted cyclopentadienyl groups, e.g. groups carrying pendant or fused substituents optionally linked together by bridging groups. Suitable metallocenes and aluminoxane cocatalysts are widely described in the literature, e.g. the patent publications of Borealis, Hoechst, Exxon, etc.

Typically however the HDPE will be prepared using multistage polymerization using a single catalyst system or a plurality of catalyst systems, e.g. two or more metallocenes, one or more metallocenes and one or more Ziegler-Natta catalysts, two or more chromium catalysts, one or more chromium catalysts and one or more Ziegler-Natta catalysts, etc.

The use of bimodal HDPE in the production of relatively large, ie. 2 to 1000L, e.g. 2 to 250L, preferably 8 to 240L, more preferably 20 to 230L, and still more preferably 30 to 225L, containers results in

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surprisingly increased values for ESCR. Thus for example tests comparing containers made using conventional monomodal HDPE with bimodal HDPE have shown an increase in ESCR F_{50} from 250 hours to over 1000 hours. (ESCR F_{50} is measured as the time taken for 50% of samples to be broken when bent and contained in a detergent solution. The test is a standard one categorised as ESCR, ASTM D-1693 condition B, 10% Igepal). Such F_{50} values for relatively large containers are particularly surprising in view of the relatively low F_{50} values (ca. 400 h) achieved for small (0.45L) containers using blow-moulding of bimodal HDPE in EP-A-778289.

The bimodal HDPE used in the process of the invention preferably has the following characteristics
Density: 940 to 970, preferably 945 to 960 kg/m³;
Weight Average Molecular Weight (Mw): 200000 to 450000, preferably 250000 to 350000 Dalton;
Number Average Molecular Weight (Mn): 6000 to 20000, preferably 7000 to 18000 Dalton;
MFR₂₁: 2 to 12 g/10 min, preferably 3 to 8 g/10 min;
Molecular Weight Distribution (i.e. Mw/Mn): 15 to 55, preferably 18 to 50;
Tensile Modulus: at least 900 mPa;
Comonomer Content: 0.5 to 10% wt, preferably 1 to 2 wt %.

MFR₂ and MFR₂₁ are routinely measured according to ISO 1133 at 190°C under 2.16 and 21.6 kg loads respectively. Tensile modulus may be measured according to ISO 527.2.

Bimodal HDPE having such characteristics may be prepared by the technique described in EP-B-517868 or by conventional use of Ziegler Natta, metallocene or chromium catalysts. Especially preferably the bimodal HDPE is produced using a series of two or more reactors, in particular a loop reactor followed by one or more gas phase reactors, preferably using a Ziegler-Natta

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polymerization catalyst.

The polymer used according to the invention preferably contains a high molecular weight component (e.g. with a molecular weight tail of about 5000000 Daltons) to increase melt strength of the HDPE composition under elongational deformation. This can be achieved in one of several ways, e.g.

(i) produce the HDPE in a multistage polymerization in which reactor conditions are set such that a very high molecular weight component is produced in one stage, e.g. by performing one reaction stage in the absence of chain terminating hydrogen, by selection of a catalyst system which produces a high molecular weight polyethylene, by use of polyenic comonomers (e.g. dienes) which produce long chain branching or otherwise promote production of a high molecular weight fraction; or

(ii) crosslinking of a polymer by timed addition of crosslinking agents in the extruder whereby to tailor-make a high molecular weight grade (i.e. to add a HMW "tail" to the polymer).

Viewed from a further aspect the invention provides a blow-moulded banded HDPE container having a volume of at least 2L (preferably 8 to 240L, etc), and an ESCR F_{50} of at least 500 hours, preferably at least 800 hours, more preferably 1000 hours, e.g. 1000 to 2000 hours.

The containers of the invention may be produced in conventional blow-moulding apparatus.

It will be appreciated therefore that the containers of the invention may be produced without loss of the impact strength or ESCR properties using faster than normal blowing rates, ie. with more efficient and economical usage of the blow moulding apparatus.

The containers of the invention may be used indoors or out of doors for storing gases, liquids or solids, especially liquids such as water, glues, solvent-based soaps, paints, varnishes, chemical solutions, oils and

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other liquid chemicals. The containers may be open (e.g. tanks, basins, etc) or may be closed, for example with lids or caps or inlet or outlet ducts.

The invention will now be described further with reference to the following non-limiting Examples.

EXAMPLE 1

Catalyst Preparation

8.6g (66.4 mmol) of 2-ethyl-1-hexanol was added slowly to 27.8g (33.2 mmol) of 19.9% butyl-octyl-magnesium. The temperature was kept below 35°C

3.7g (1.0 mmol/g carrier) of 20% EADC (ethyl aluminium dichloride) was added to 5.9g of Sylopol 5510 silica/MgCl₂ carrier and the mixture was stirred for 1 hour at 30°C. 5.7g (0.9 mmol/g carrier) of the 2-ethyl-1-hexanol/butyl-octyl-magnesium complex was added and the mixture was stirred for 5 hours at 45°C. 0.6g (0.55 mmol/g carrier) of TiCl₄ was added and the mixture was stirred for 5 hours at 45°C. The catalyst was dried at 45-80°C for 3 hours.

EXAMPLE 2

Bimodal HDPE Polymer Preparation

Ethylene, propane and hydrogen were introduced at 2.4 kg/hour, 25 kg/hour and 1 g/hour respectively into a 50 dm³ slurry loop reactor operated at 85°C and 65 bar. The catalyst of Example 1 was introduced at a rate sufficient to produce polyethylene (PE) at about 1.9 kg PE/hour. The MFR₂ and density of the PE product were estimated to be about 10 g/10 min and 970 kg/m³ respectively. The slurry was withdrawn continuously and

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introduced into a second loop reactor of volume 500 dm³, operating at 95°C and 61 bar. Additional ethylene, propane and hydrogen were added to produce a PE of MFR₂ 330 g/10 min and density 974 kg/m³ at 30 kg PE/hour. The polymer, which contained the active catalyst, was continuously withdrawn, separated from the reaction medium and transferred to a gas phase reactor. Here additional ethylene, hydrogen and 1-butene comonomer were added to produce a PE of MFR₂₁ 7.3 g/10 min and density 949 kg/m³ at 69 kg PE/hour. The low MW (high MFR) fraction thus represented 45% of the total polymer.

EXAMPLE 3

Bimodal HDPE Polymer Production

Polymerization was effected as in Example 2 except that 36 kg PE/hour was formed in the second loop reactor, 77 kg PE/hour was formed in the gas phase reactor and the MFR₂₁ and density of the final PE were 3.3 g/10 min and 952 kg/m³ respectively. The low MW (high MFR) fraction represented 48% of the total polymer.

EXAMPLE 4

Bimodal HDPE Polymer Production

Ethylene, propane and hydrogen were introduced into a 50 dm³ slurry loop reactor operating at 80°C and 65 bar at 2.0 kg/hour, 28 kg/hour and 1 g/hour respectively. A catalyst according to Example 3 of EP-B-688794 was added to produce PE at a rate of 1.6 kg PE/hour. The MFR₂ and density of the PE were estimated to be about 10 g/10 min and 970 kg/m³ respectively. The slurry was continuously withdrawn and introduced into a second loop reactor of 500 dm³ volume operating at 95°C and 61 bar. Additional ethylene, propane and hydrogen were added so that the

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second loop reactor produced PE at a rate of 34 kg PE/hour with MFR₂ and density of 55 g/10 min and 970 kg/m³ respectively. PE polymer, containing the active catalyst, was withdrawn continuously from the second loop reactor, separated from the reaction medium and transferred to a gas phase reactor where additional ethylene, hydrogen and 1-butene comonomer were added such that PE was produced at 70 kg PE/hour with MFR₂₁ and density of 6.9 g/10 min and 948 kg/m³ respectively. The fraction of low MW (high MFR) polymer was thus 50%.

EXAMPLE 5

Bimodal HDPE Polymer Production

Polymerization was effected as in Example 4 except that 38 kg PE/hour and 78 kg PE/hour were formed in the second loop reactor and the gas phase reactor respectively. The final PE had MFR₂₁ and density of 7.3 g/10 min and 948 kg/m³ respectively and the low MW fraction was 50%.

EXAMPLE 6

Blow Moulding

30L containers were blow moulded on a Krupp Kautex KB50 blow moulding machine at an extruder temperature of 210°C using the HDPE polymers of Examples 2 to 5. The containers were pre-stored at 42°C for 3 weeks containing n-butyl acetate. The n-butyl acetate was replaced with ethylene glycol and the containers were cooled to -20°C within 24 hours and drop-tested at -20°C using the test method of ASTM 2463-90, giving values of 2 to 3.25 m. The ESCR F₅₀ values were also determined using ASTM D1693, condition B.

EXAMPLE 7Polymer Properties

The measured properties of the polymers of Examples 2 to 5 and a comparison PE prepared using a chromium based catalyst are set out in Table 1 below. The comparison PE is commercially available as HE8214 from Borealis AS.

Property	Example 2	Example 3	Example 4	Example 5	HE 8214
MFR ₂₁ (g/10 min)	7.3	3.3	6.9	7.3	2.7
Density (kg/m ³) *	948.5	951.5	947.9	948	950.4
Mw	260000	370000	305000	316000	345000
Mn	8300	7700	12000	16000	16000
MWD	31	48	25	20	22
Tensile Modulus (mPa)†	920	1030	920	910	1065
ESCR F50 (hours)	542	>1000	>1000	>1000	391
Comonomer	1-butene	1-butene	1-butene	1-butene	1-hexene
Comonomer content (% wt)	1.8	1.1	1.4	1.2	<0.1

* ISO 1183

† ISO 527-2

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Claims

1. A process for the preparation of at least 2L volume polyethylene container which process comprises blow moulding a bimodal HDPE, wherein said HDPE contains an ethylene homopolymer and an ethylene copolymer.
2. A process as claimed in claim 1 wherein said HDPE contains an ethylene homopolymer having a weight average molecular weight of 20000 to 40000 D.
3. A process as claimed in either of claims 1 and 2 wherein said HDPE has a density of 945 to 975 kg/m³.
4. A process as claimed in any one of claims 1 to 3 wherein said HDPE has a density of 945 to 960 kg/m³, a weight average molecular weight of 250000 to 350000 D, a number average molecular weight of 7000 to 18000 D, a molecular weight distribution of 18 to 50, an MFR₂₁ of 3 to 8 g/10 min, a tensile modulus of at least 900 mPa, and a comonomer content of 1 to 2 wt. %.
5. A blow-moulded bimodal HDPE container having a volume of at least 2L, and an ESCR F₅₀ of at least 500 hours, wherein said HDPE contains an ethylene homopolymer and an ethylene copolymer.
6. A container as claimed in claim 5 having a volume of at least 8L.
7. A process as claimed in claim 1 wherein said bimodal HDPE has the following characteristics:
a density of 940 to 970 kg/m³;
a weight average molecular weight of 200000 to 450000 D;
a number average molecular weight of 6000 to 20000 D;
a molecular weight distribution of 15 to 55;
MFR₂₁ of 2 to 12 g/10 min;

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tensile modulus at least 900 mPa; and
a comonomer content of 0.5 to 10 wt%.

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ABSTRACT

The invention provides the use of bimodal HDPE in the production by blow moulding of medium to large volume containers having improved environmental stress crack resistance.

Declaration and Power of Attorney

U.S. Serial No. 10/049,879

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I hereby claim the benefit under Title 35, United States Code, § 120 of any United States application(s) or § 365(c) of any PCT international application designating the United States of America, listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States or PCT International application in the manner provided by the first paragraph of Title 35, United States Code, § 112, I acknowledge the duty to disclose information which is material to patentability as defined in Title 37, Code of Federal Regulations, § 1.56 which became available between the filing date of the prior application and the national or PCT international filing date of this application (37 C.F.R. § 1.63(d)).

PCT/ GB00/03149

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

I hereby authorize my attorney to insert the serial number assigned to this application in this declaration should this number become available before the filing of this declaration.

POWER OF ATTORNEY: As a named inventor, I hereby appoint the practitioners associated with the firm of LINIAK, BERENATO, LONGACRE & WHITE, LLC to prosecute this application and to transact all business in the Patent and Trademark Office connected therewith, and direct that all correspondence and telephone calls be addressed to:

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DECLARATION FOR PATENT APPLICATION AND APPOINTMENT OF ATTORNEY

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DECLARATION FOR PATENT APPLICATION AND APPOINTMENT OF ATTORNEY

As a below named inventor, I hereby declare that my residence, post office address and citizenship are as stated below next to my name; I believe that I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled:

CONTAINER PRODUCTION PROCESS

the specification of which (check one):

() is attached hereto, or () was filed on: 19 February 2002

as U.S. Application Serial No. 10/049,879 or PCT

International Application No.:

and (if applicable) was amended on:

I hereby state that I have reviewed and understand the contents of the above-identified specification, including the claims, as amended by any amendment(s) referred to above. I acknowledge the duty to disclose information which is material to patentability as defined in *Title 37, Code of Federal Regulations, § 1.56*. I hereby claim foreign priority benefits under *Title 35, United States Code, § 119* of any foreign application(s) for patent or inventor's certificate listed below and have also identified below any foreign application for patent or inventor's certificate having a filing date before that of the application on which priority is claimed:

PRIOR FOREIGN APPLICATION(S)			PRIORITY CLAIMED	
Number	Country	Day/Month/Year Filed	Yes	No
9919718.8	GB	19 August 1999	✓	